

Photo Catalytic Degradation of Effluent of Iron and Power Plant Industries in Aqueous Solution by ZnO Nano Catalyst Using UV Irradiation

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Abstract: Photo catalysis of organic compounds in water is receiving attention due to the severe ecological impact of various industrial and agricultural pollutants. Photo catalytic activities can be classified into homogeneous or heterogeneous reactions depending on the nature of their reactants and materials (semiconductors). Particularly, heterogeneous photo catalytic study using semiconductor materials such as TiO₂ and ZnO, through particulate systems, has become an exciting and rapidly growing area of research in the last few years mainly due to the relatively simple photodecomposition of organic pollutant molecules into less harmful compounds. The iron and power plant industries consume significant amount of water during the power generation and finishing operations. In this operation a used water having high chemical oxygen demand contents and the waste water discharged in rivers or public sewage treatment plant. Their treatment has been a necessary aspect for human prosperity and ecological environment. This paper shows the detailed study of photo catalytic degradation of effluent carried out in the presence of an aqueous solution of ZnO nano catalyst irradiated with UV light in a batch reactor. It was observed that photo catalytic degradation of effluent obey pseudo first order kinetics according to Langmuir-Hinshelwood model. The influences of various factors in rate of reaction are, initial effluent concentration, catalyst concentration and UV light irradiation time on degradation efficiency were scientifically studied. The degradation of effluent was determined by Photo colorimeter and determines the COD degradation through transmittance of effluent.

Keywords: Photo catalytic degradation, ZnO nano catalyst, COD, AOP's, Iron and power plant waste water.

I. Introduction

A wide variety of organic pollutants are introduced into the water system from various sources such as industrial effluents, agricultural runoff and chemical spills (Muszkat et al., 1994; Cohen et al., 1986). Their toxicity, stability to natural decomposition and persistence in the environment has been the cause of much concern to the societies and regulation authorities around the world (Dowd et al., 1998).

Environmental pollution is produced either by a natural source or by some anthropogenic activity, or by human. Which has an adverse effect on humans, animals, plants and materials? The inordinate population growth, fast industrialization, rapid urbanization and modified agricultural operations have intensified the pollution of air and water both and as a consequence, the human health is seriously affected by this environmental and ecological disorder. If this situation is not controlled timely, it would become a malignant problem for the survival of mankind on this planet. Environment pollution by organic pollutant also sets several ecological problems, which is increased by the fact that most of them are difficult to degrade using standard biological methods. For the removal of such recalcitrant pollutants some traditional, physical techniques such as adsorption on activated charcoal, ultra filtration, reverse osmosis and coagulation is used efficiently. Nevertheless they are nondestructive. Recently there has been considerable interest on the utilization of advanced oxidation process (AOPs) for the destruction of organic compounds in contaminated water.

Semiconductor particles have been found to act as heterogeneous photocatalysts in a number of environmentally important reactions (Blake, 2001; Pirkanniemi, & Sillanpää, 2002; Gaya & Abdullah, 2008). Materials such as colloidal TiO₂ and ZnO have been found to be efficient in laboratory-scale pollution abatement systems (Barni et al., 1995; Bellobono et al., 1994; Legrini et al., 1993; Mills & Hunte, 1997; Halmann, 1996), reducing both organic [e.g. halogenocarbons (Gupta & Tanaka, 1995; Martin et al., 1994; Read et al., 1996;), benzene derivatives (Blanco et al., 1996; Mao et al., 1996) detergents (Rao & Dube, 1996), PCB's (Huang et al., 1996), pesticides (Gianturco et al., 1997;)

The key advantage of this degradation method is that it can be carried out under ambient condition and lead to complete degradation of organic compounds. Among the advanced oxidation process heterogeneous photo catalysis appears as an emerging technology leading to the total mineralization of most of the organic pollutants. If a suitable semiconductor is irradiated with visible or UV light electron excitation from Valance band to conduction band results and a vacancy or hole is left in the valance band such holes have the effect of a positive charge. Thus in turn generates the formation of "holes" on the surface of the semiconductor, which

can react with oxygen, water and hydroxide ion to form hydroxyl radicals. Furthermore, super oxide radicals are formed from the reaction of excited electrons with oxygen molecules. The highly reactive oxygen species so formed react with the organic pollutants resulting in their oxidation.

The kinetics of photo catalytic degradation of many organic compounds in ZnO suspensions under visible irradiation has often been matched to the simple langmuir-hinshelwood equation -1

$$r = -dc/dt \quad \dots\dots \text{equation-1}$$

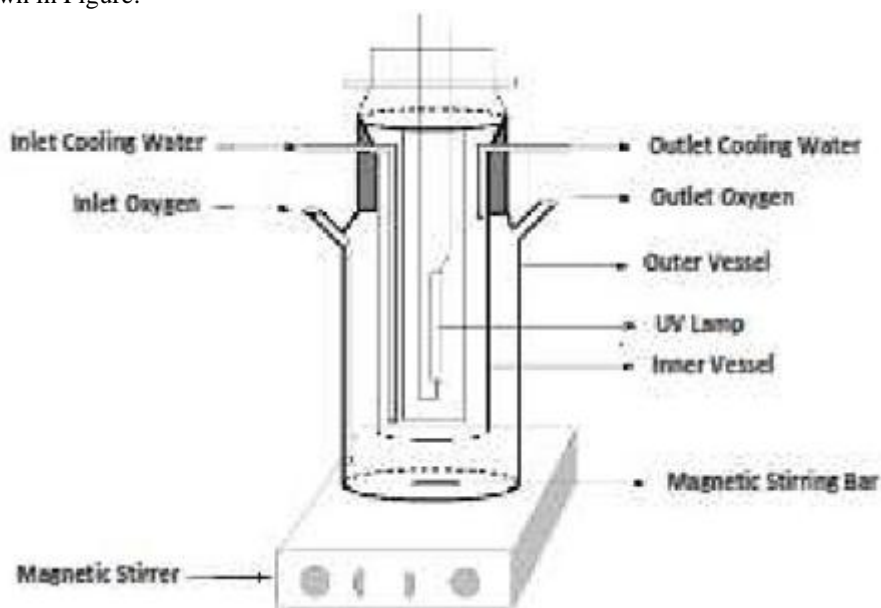
Where K' is the apparent rate constant of photo catalytic degradation. The plot of (C0/C) Vs time yield a straight line and its slop is Kr' in equation -2

$$t^{1/2} = 0.693/K' \quad \dots\dots \text{equation 2}$$

II. Method And Material

Procedure for conducting the degradation experiments

Stock solutions of the pollutants containing the desired concentration were prepared in double distilled water. An immersion well photochemical reactor made of Pyrex glass equipped with a magnetic stirring bar, water circulating jacket and an opening for supply of molecular oxygen was used. A simplified diagram of the reactor system is shown in Figure.



ZnO AS PHOTO CATALYST

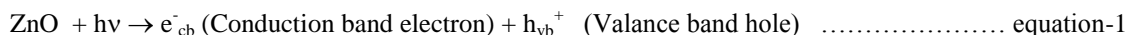
ZnO is a semiconductor used as photo catalyst in various photo catalytic reactions. Generally semiconductors have large band gaps are good photo catalyst. ZnO and TiO₂ with band gaps larger then 3ev show strong (shown in table-1) activity. The conduction and valance band potentials of both TiO₂ and ZnO are larger than the corresponding redox potentials of H⁺/H₂ and H₂O/O₂ and the photo generated electron and hole can be separated efficiently. Photo catalytic mechanism of ZnO nano catalyst show in below

Table-1

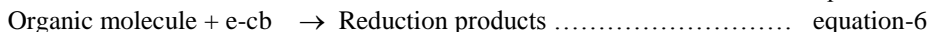
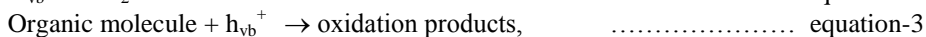
Photo Catalyst	Band gap (ev)
ZnO	3.2
TiO ₂	3.1
CDS	2.3
α-Fe ₂ O ₃	2.3

Chemistry of Photo Catalytic Reaction

When photo catalyst nano catalyst absorb the ultraviolet light from sun light or different sources ,then it will produce a pair of electron and holes .The valance electron of ZnO are become excited when they get the energy from UV light or illuminated by sources. If the energy of excited electron is greater than the threshold energy then electron goes to valance to conduction band of ZnO and create the negative electron and positive-hole pair. The stage is referred as semiconductor photo excitation stage. Positive holes of ZnO break apart the water molecule to form hydrogen gas and hydroxyl radical and the negative electron react with oxygen molecule and form super oxide anion, This cycle continue when light is available.



Due to the higher band gap ZnO can be activated only by UV irradiation of wavelength below 385 nm. The photo generated valance band hole and valance band electrons can either recombine to liberated heat, or make their own ways to the surface of ZnO, where they can react with species absorbed on the surface of catalyst shown in Equation 3 and 6.



Hydroxy radical HO^\bullet , along with per hydroxyl radical HO_2^\bullet can oxidise the most of the organic molecule and reduce the organic load in waste water.

III. Result And Discussion

Experimental Set Up

Chemicals – all chemicals are of AR grade potassium dichromate, Sulphuric acid and mercuric sulfate was used. The photo catalyst ZnO nano catalyst was used.

Experimental Procedure

The photo catalytic reaction was carried out in a batch reactor with dimension of 7.5 X 6 cm (height X diameter) provide with a water circulation arrangement in order to maintain the temperature in the range of 25 – 30° C. The irradiation was carried out using 500W halogen lamp. In all cases during the photolysis experiments the effluent, Potassium dichromate, sulphuric acid and mercuric sulphate solution and the catalyst was placed in the reactor and stirred magnetically with simultaneously exposure to visible light. Sample was withdrawn at periodic intervals from the reactor to assess the extent of de-colorization. The intensity of light was measured by lux meter (Lutron LX-101). A photocolormetr was used for measuring absorbance at different time intervals at 620 nm.

Effect of Concentration of effluent

Photo catalytic degradation of effluent for different concentration of effluent like 10mL, 15 mL, 20 mL, 25 mL and 30 mL solution containing 30 mg ZnO nano catalyst. The change in concentration of the effluent in the solution, plotted as function of concentration of effluent. It is seen that degradation of COD value was increase with time. Table- 1 shows the k value of COD degradation when concentration of catalyst is constant and effluent concentration are changed.

An aliquot of 3.0 ml was taken out from the reaction mixture at regular time intervals and the absorbance was measured at $\lambda_{max} = 620 \text{ nm}$. It was observed that the absorbance of the solution decreases with increasing time intervals, which indicates that the concentration of COD decreases with increasing time of exposure. A plot of transmittance verses time was linear and follows pseudo first order kinetics. The rate constant was measured using following expression:

$$k = 2.303 \times \text{slope}$$

The results of typical run for photo catalytic degradation of COD are shown in the Table 1 and graphically represented in Fig 1.

Amount of ZnO = 30mg

Light intensity = 17500 lux

$\lambda_{max} = 620 \text{ nm}$

[Effluent Concentration = 10 ml]

Table 1- Effect of sample concentration

Sample Concentration In mL	K value/sec
10	94.95
15	135.65
20	143.53
25	163.98
30	177.18

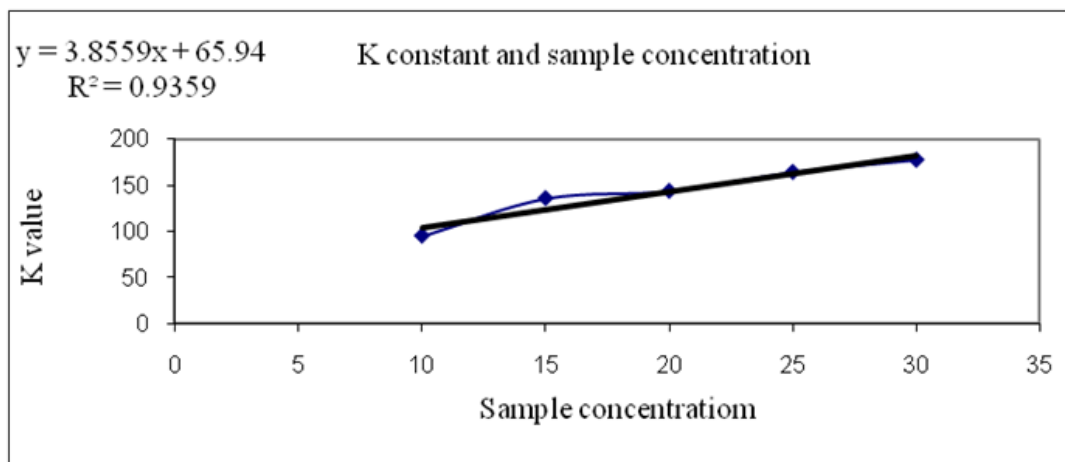


Fig-1

Concentration of catalyst

The effect of concentration of catalyst on the rate of photo catalytic degradation was observed by taking different concentrations of catalyst and effluent concentration was constant. The results are reported in the table 2. It is obvious to expect increase in reaction rate. It is evident that as the concentration of catalyst was increased, the rate of photo catalytic degradation of COD was increased.

From the experimental result we have observed that the decrease of k value with increase in initial concentration of the sample and vice versa can be attributed to the decrease in the path length of photon entering the solution due to impermeability of the solution. At low concentration the reverse effect observed, hereby increasing the number of photon absorption by the catalyst. This decreasing phenomenon can further be explained in terms of the increase in requirement of catalysts surface for the increased concentration of the sample. But here the amount of catalyst had been kept constant. Hence the relative number of O_2^{\bullet} and OH^{\bullet} radicals formed on the surface of ZnO are also constant. As a result the relative number of O_2^{\bullet} and OH^{\bullet} attacking the organic molecule with increasing initial concentration of the catalyst. The plot of CO Vs k should yield a straight line. The k_r and k values were calculated from slope of the straight line and intercept respectively. Amount of ZnO = 30mg, 60mg, 90mg, 120 mg, 150 mg,

Light intensity = 17500 lux λ_{max} =620nm

Table 2 - Effect of catalyst concentration

Catalyst In mg	K Value/sec
30	116.82
60	88.99
90	70.45
120	53.52
150	48.24

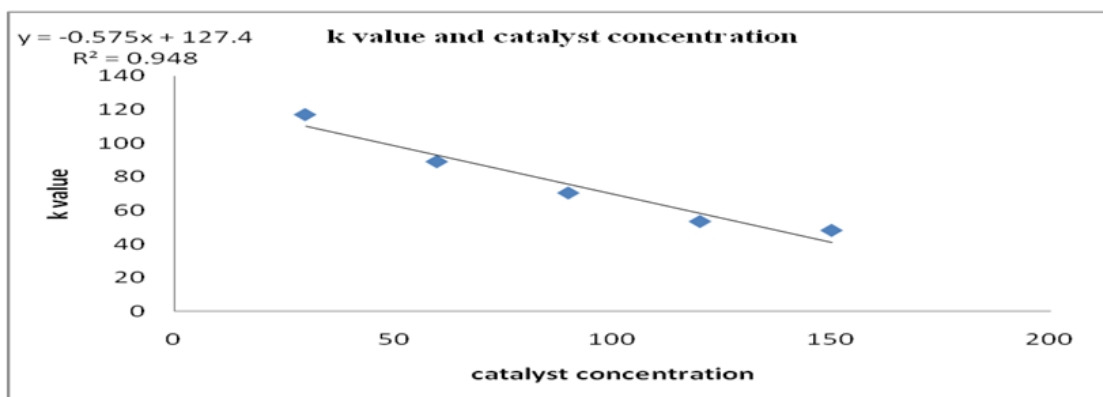


Fig-2

Effect of sample concentration on reaction rate

In X axis represent the Time and Y axis % transmittance.

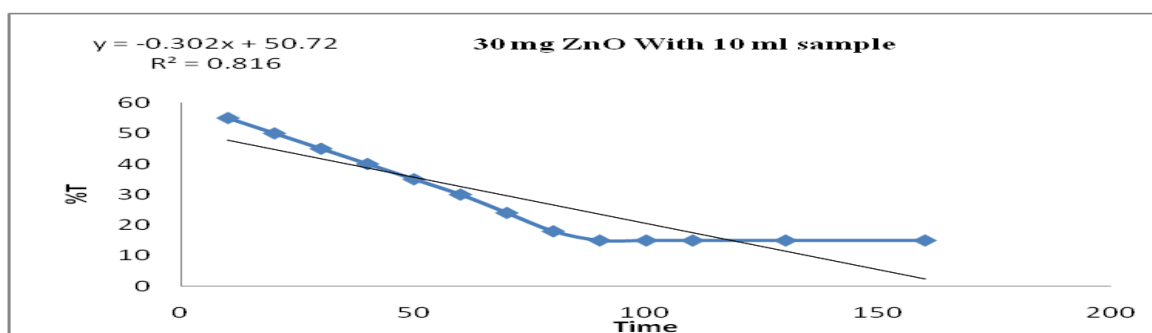


Fig-3

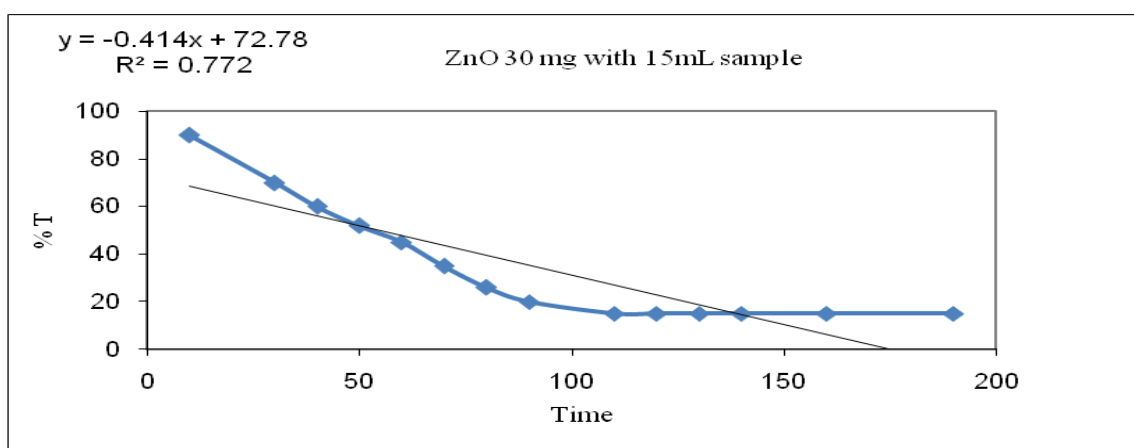


Fig-4

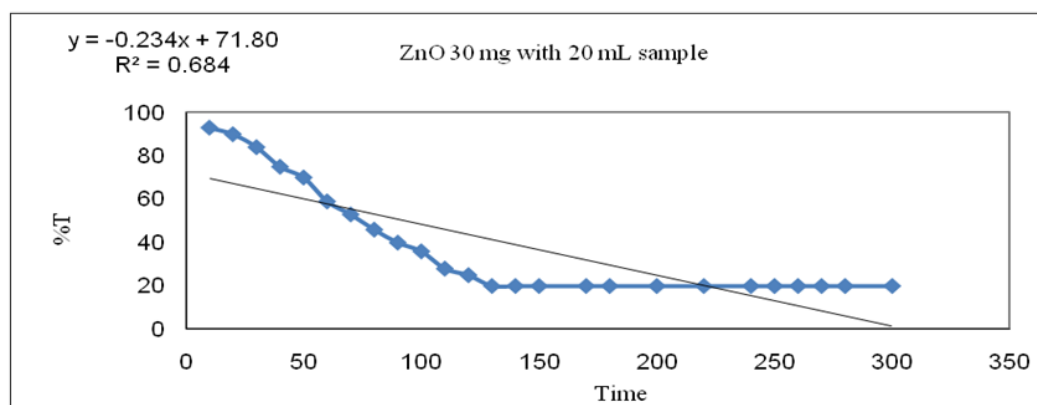


Fig-5

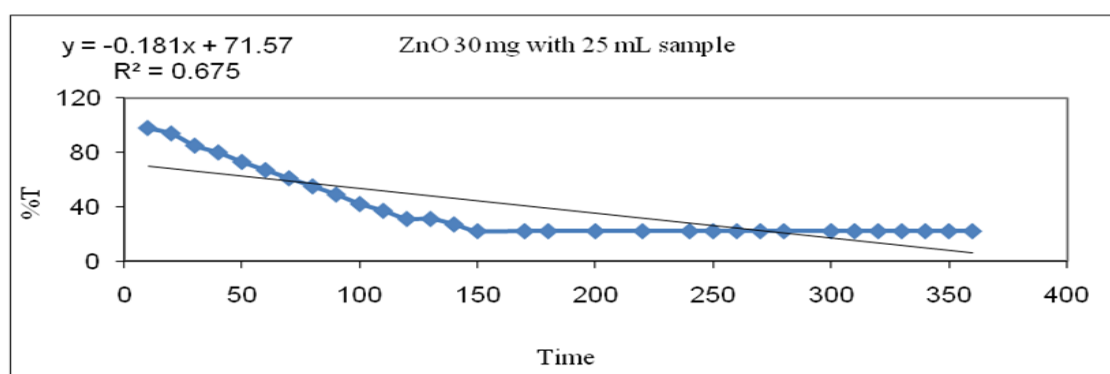


Fig-6

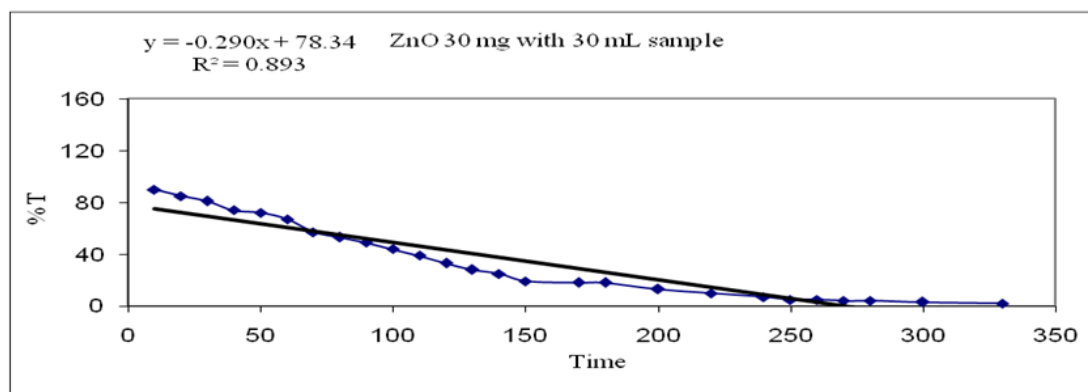


Fig-7

Effect of Catalyst concentration on reaction rate:

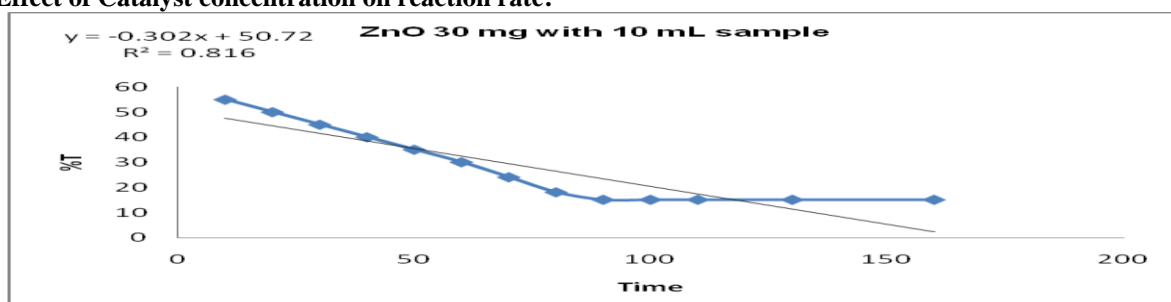


Fig-8

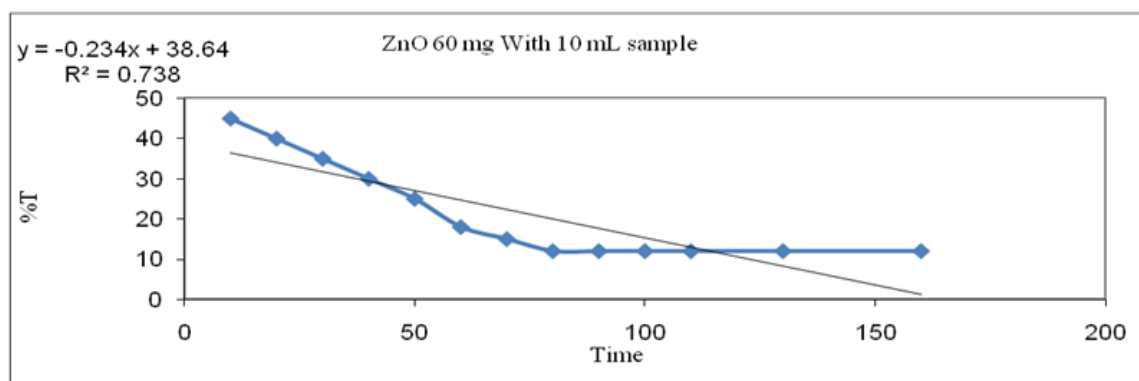


Fig-9

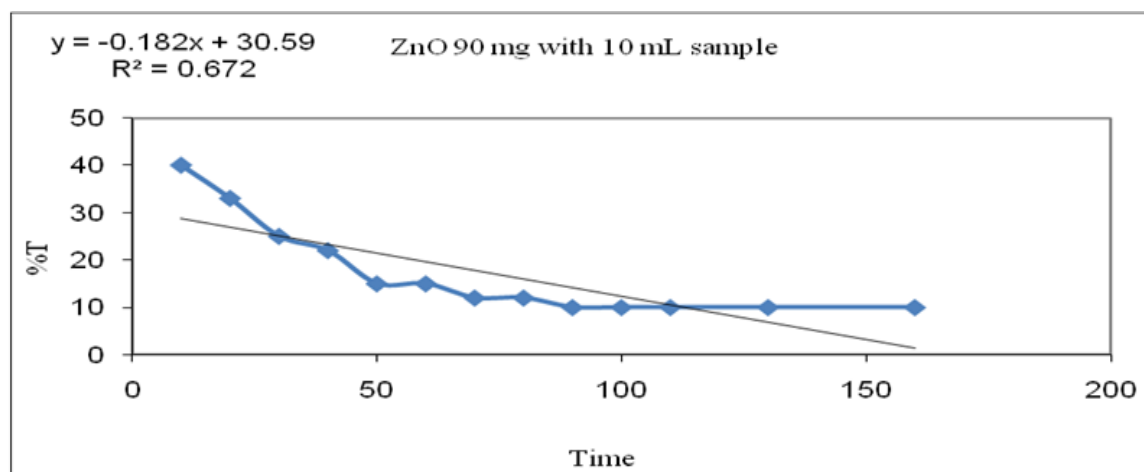


Fig-10

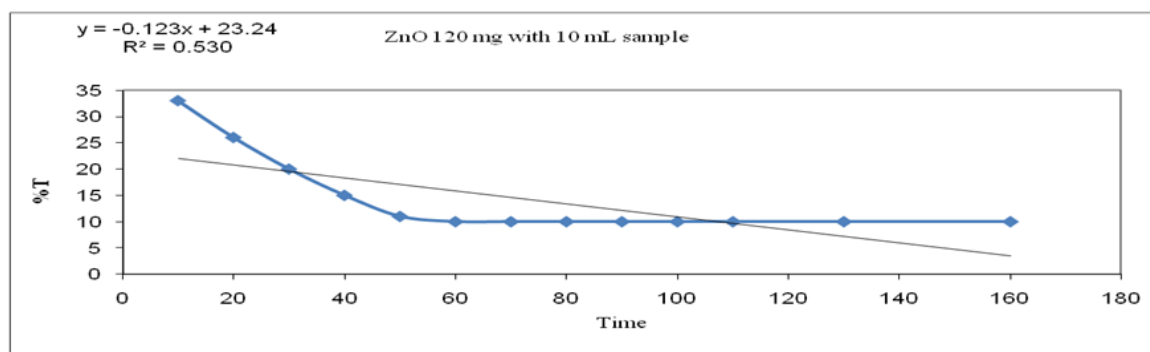


Fig 11

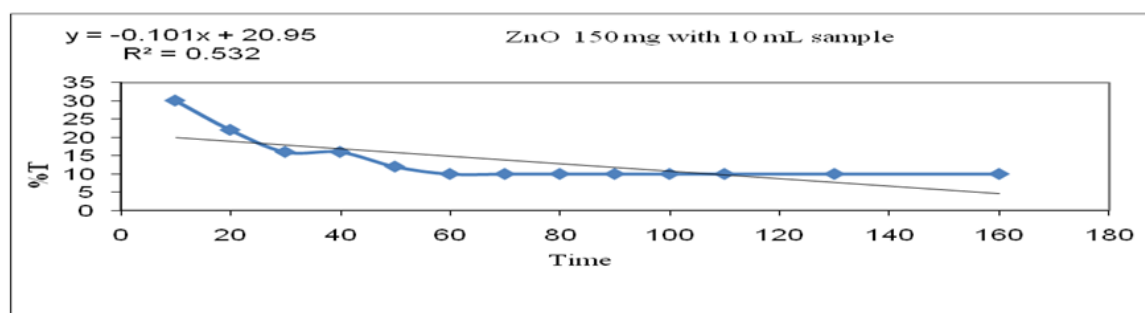


Fig 12

IV. Conclusion

This paper describes the degradation of organic molecule through ZnO nano catalyst/UV and this is pseudo first order kinetics, the kinetics of heterogeneous catalytic (ZnO) reaction applied to waste water treatment. It's a novel experiment for the determination of the kinetics of photo catalytic degradation of organic molecule (COD) in aqueous solution. It further validates the importance of AOPs in degradation of waste water. In this method organic molecule are completely degraded through nano catalyst.

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